



# Optimizing productivity on high capacity protein A affinity medium

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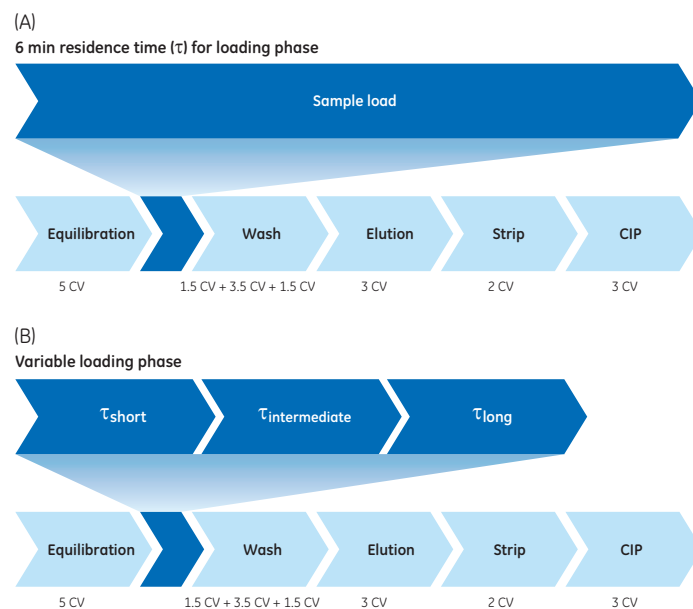
# Optimizing productivity on high capacity protein A affinity medium

MabSelect SuRe™ protein A affinity medium has long been considered a standard tool for capturing monoclonal antibodies (MAbs) in biopharmaceutical production. Utilizing the same alkali stable ligand, MabSelect SuRe LX has very high dynamic binding capacity and has been developed for high titer antibody processes. To achieve optimal performance, MabSelect SuRe LX is best operated at 6 min residence time during load. This Application Note summarizes studies on designing customized loading strategies to shorten the average residence time when using MabSelect SuRe LX with the goal of improving productivity (calculated as the amount of MAb purified per volume medium and time) even further, without affecting capacity. By using variable residence times (including residence times shorter than 6 min) during the loading phase, productivity over the cycle was increased by nearly 40%, relative to a reference run at a single residence time. In addition, theoretical studies, based on knowledge of the shape of the curve of dynamic binding capacity (DBC) on residence time, showed almost identical results as obtained in the experimental studies.

MabSelect SuRe and MabSelect SuRe LX are BioProcess™ protein A chromatography media specifically made to fulfill the performance specifications and batch-to-batch reproducibility required in downstream processing. MabSelect SuRe LX has the same base matrix and the same ligand as MabSelect SuRe - the difference is higher ligand density for MabSelect SuRe LX, enabling higher capacities. The higher capacity for MabSelect SuRe LX is reached at 6 min residence time (RT) during loading, which are normal loading times in industrial applications. The goal with this study was to investigate the possibility to reduce residence time during load by designing an innovative loading strategy to improve the productivity even further, without significantly affecting capacity.

One way to address this is to use variable RTs during the loading phase. This involves dividing the loading step into several steps, with variable RTs and flow rates (Fig 1). Using variable RTs during loading is not a new concept (1), but the high dynamic binding capacity at longer RTs allows for new possibilities when using MabSelect SuRe LX.

Variable loading approach has also been shown to improve the binding capacity of MabSelect SuRe LX medium (2).



**Fig 1.** Graphic representation of (A) single RT over loading phase and (B) variable RT over loading phase. For all non-loading phases, 2.4 min residence time is used, except first post-load wash step (1.5 CV, 6 min), elution (4 min) and CIP (5 min).

The productivity optimization procedures described in this Application Note involve four main steps: 1) determination of DBC at various RTs, 2) determination of optimal RT during load, 3) experimental analyses using Design of Experiments (DoE), and 4) theoretical modelling. Theoretical modelling was performed to evaluate the possibility to optimize the variable RT over a minimum number of experiments.

## Product characteristics

### MabSelect SuRe and MabSelect SuRe LX

MabSelect SuRe is a recombinant protein A based affinity medium, designed for the capture of MABs at process scale. Its optimized, cross-linked high flow agarose matrix gives at least five times higher fluid velocities as compared to conventional cross linking. MabSelect SuRe has an alkali-tolerant rProtein A ligand that allows the use of rigorous and cost-effective cleaning-in-place (CIP) and sanitization protocols based on 0.1 to 0.5 M NaOH. Further, the ligand is protease stable, leading to lower ligand leakage.

MabSelect SuRe LX delivers very high dynamic binding capacity at extended RTs and was developed for high titer antibody processes. Alkali tolerance, high capacity, and low ligand leakage, in combination with the rigid base matrix makes MabSelect SuRe LX an excellent choice for purification of MABs for a wide variety of applications.

## Methods

### DBC at different RTs

The first step in the optimization procedure is to establish dynamic binding capacity at different RTs. Tricorn™ (5 × 100 mm) columns were packed with 2 mL MabSelect SuRe LX (10 cm bed height) and loaded with MAb-containing harvested cell culture fluid (HCCF). Fractions were collected during load and analyzed with a Biacore™ T200 system RT was varied at 1, 1.2, 2, 3, 4, 5, 6, and 10 min, and 10% breakthrough capacity ( $Q_{b,10}$ ) was determined for each RT. All RT experiments were performed on ÄKTA™ systems.

### Chromatography method for DBC measurement

The column was first equilibrated with 5 column volumes (CV) of 20 mM sodium phosphate, 150 mM sodium chloride (NaCl) and the cell culture supernatant was subsequently loaded at the respective RTs. When the breakthrough occurred the unbound material was washed out with equilibration buffer. The bound MAb was eluted with 5 CV of 100 mM acetic acid and the column was neutralized with equilibration buffer prior to CIP with 0.1 M NaOH for 15 min before the column was re-equilibrated with equilibration buffer.

### Optimizing the combination of RT during load

Based on the DBC at different RTs, an optimization analysis was performed using Modde™ (Umetrics) DoE software (see Table 1). A combination of three RTs was chosen: the last was fixed to 6 min while the first two were optimized for the shortest average RT. Short RT will give the best productivity provided the capacities are kept constant.

Table 1. DoE layout for determining optimal RTs

Experiment number	Run order	RT 1 (min)	RT 2 (min)	RT3 (min)
1	9	1.2	2.5	6
2	1	2.0	2.5	6
3	2	1.2	4.5	6
4	8	2.0	4.5	6
5	6	1.2	3.5	6
6	10	2.0	3.5	6
7	5	1.6	2.5	6
8	4	1.6	4.5	6
9	7	1.6	3.5	6
10	3	1.6	3.5	6

### Chromatography method for variable RTs

The column was first equilibrated with 5 CV of 20 mM sodium phosphate, 150 mM NaCl and the cell culture supernatant was then loaded at the shortest RT (RT1), followed by the intermediate RT (RT2), and then the final RT (RT3) of 6 min. For all RTs the column was loaded to 80% of  $Q_{b,10}$  for the respective RT. After completing the load the column was washed with equilibration buffer. Once the UV signal had returned to 200 mAU, the flow rate was increased and washing continued until a total of 5 CV of equilibration buffer was passed over the column. This was followed by an intermediate wash using 100 mM sodium acetate (pH 6) for another 1.5 CV, before the elution with 100 mM acetic acid. The elution peak was collected between 100 mAU and 100 mAU and when the collection had finished, another 2 CV of elution buffer was passed over the column to strip off any remaining MAb. The column was neutralized with equilibration buffer before a 15 min CIP with 0.1 M NaOH.

## Analyses

### Concentration determination of MAb

Concentration determination for the cell culture supernatant and fraction from the DBC runs were analyzed with a Biacore T200. MabSelect SuRe ligand was immobilized using EDC/NHS chemistry to a level of about 3000 RU on a CM5 chip.

Note: Biacore Sensor Chip Protein A with immobilized MabSelect SuRe ligands are now also available for purchase. These ready-to-use sensor chips, for antibody concentration and kinetic analysis, eliminate the need to develop immobilization and regeneration conditions.

### Recovery

Eluates were analyzed with size exclusion chromatography (SEC) and the returned area was compared to a standard curve obtained by injecting different amounts of the MAB reference standard on the column. The standard curve was constructed by plotting the nominal MAB concentrations versus the respective obtained total area.

## Determination of aggregate concentration

Fractions from the chromatography runs were collected and analyzed by SEC on a Superdex™ 200 Increase 10/300 GL column. The peaks were integrated and the relative aggregate concentrations (in percent) were determined

## Determination of host cell protein (HCP) and protein A content

HCP content in the elution fractions and product pools were analyzed using commercially available anti-CHO HCP antibodies (Cygnus Technologies Inc.) and Gyrolab™ workstation (Gyros AB). Protein A content was determined using a commercially available ELISA kit (Repligen Corp.).

## Charge variants

Charge variants were analyzed using a ProPac™ WCX 10 2 × 250 mm column (Thermo Fisher). The analysis was carried out on an Agilent 1260 system.

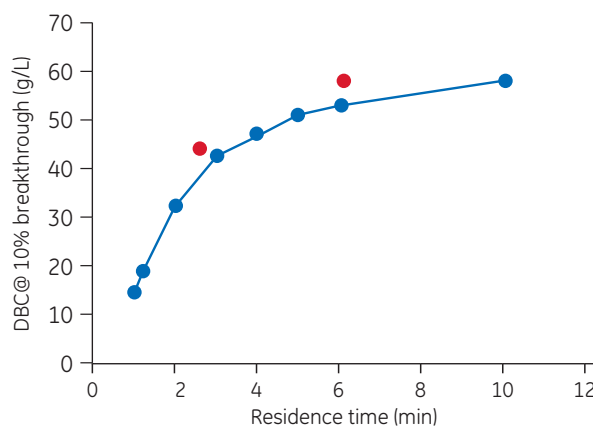
## Results

### Experimental studies

DBC for the different tested RTs varied from 15 to 58 g/L in the analyzed time range (Fig 2). When combining two relatively short RTs, 2 followed by 4 min (average RT of 2.6 min), a higher capacity was obtained relative to a single RT at 3 min. A higher capacity was also obtained when comparing a combined, longer RT (4 min followed by 10 min; average RT of 6.1 min) with a single RT at 6 min.

On average, a variable residence time run yielded 95% of the breakthrough capacity of the longest chosen residence time (e.g., a three step load where the longest time was 6 min resulted in 95%  $Q_{b,10}$  of a standard run using 6 min as the residence time).

It is the response of DBC to RT that determines the impact of the variable RT loading approach on productivity. Note that in Figure 2, the DBC continues to increase with increased RT. This response is critical if the goal is to achieve higher productivity by implementing variable RT loading. The response of DBC to RT is unique to each MAb; therefore, this curve needs to be developed experimentally. Note that the DBC obtained using variable RT loading (red dots) is consistently higher than that obtained using single RTs. This is because the variable RT technique allows for the DBC with the longest RT, while reducing the average RT for the load.



**Fig 2.** DBC at different RTs. Blue dots represent single and red dots dual (2 min followed by 4 min, and 4 min followed by 10 min) RTs. Dual RTs are plotted as the average.

### DoE for optimal RT

DoE was used to find the optimal combination of RTs to maximize the productivity for MabSelect SuRe LX (Table 2). The experiments were performed as three consecutive loadings where the RTs of the first two were varied and the third was always kept as 6 min RT.

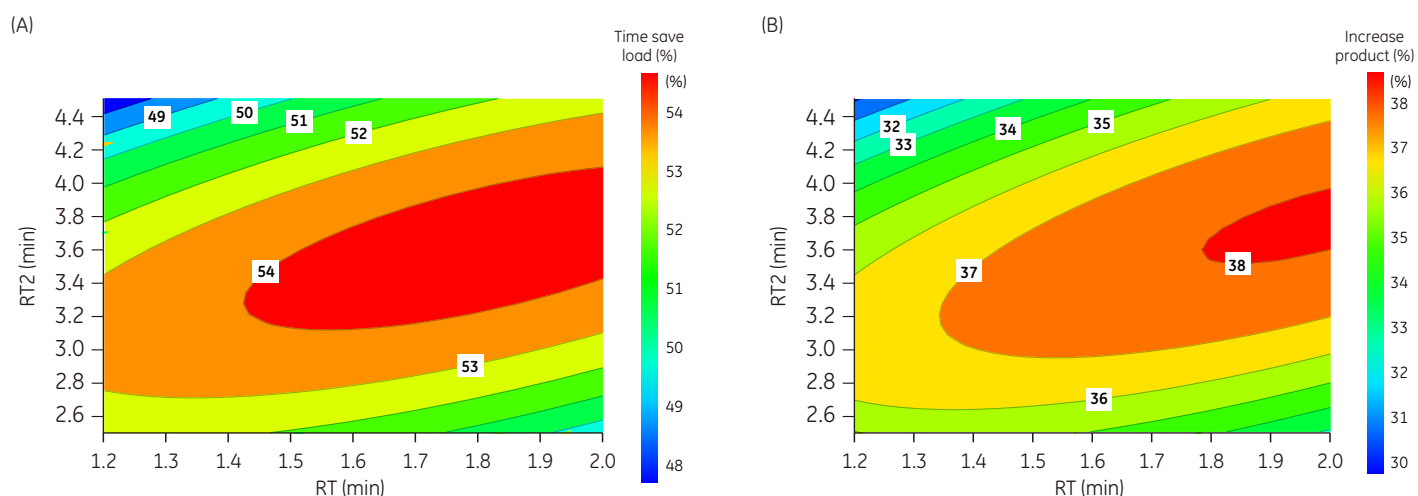
**Table 2.** Summary of DoE to optimize productivity at different combinations of RTs

Experiment number	Experiment name	Run order	RT1 (min)	RT2 (min)	RT3 (min)	Productivity (g/L/hr)	Load time (min)	Increased productivity (%)
Reference at 6 min RT	RT6	N/A	N/A	N/A	6.0	21.1	71.1	0
1	N1	10	1.2	2.5	6.0	28.5	34.0	36
2	N2	1	2.0	2.5	6.0	28.0	36.0	33
3	N3	2	1.2	4.5	6.0	27.4	37.5	30
4	N4	8	2.0	4.5	6.0	28.8	33.7	37
5	N5	6	1.2	3.5	6.0	28.6	33.4	36
6	N6	10	2.0	3.5	6.0	29.0	32.6	38
7	N7	5	1.6	2.5	6.0	28.4	34.3	35
8	N8	4	1.6	4.5	6.0	28.2	35.0	34
9	N9	7	1.6	3.5	6.0	29.0	32.5	38
10	N10	3	1.6	3.5	6.0	29.0	32.5	38

The productivity at a single residence time of 6 min was used as reference to calculate increase in productivity when performing loading at varied RTs. The DoE showed little variability in terms of productivity and load time, suggesting that the process is robust and will not be prone to large changes in productivity or process time if there are small variations in the achieved RTs. The eluates were also analysed for product quality and these results were also consistent (Table 3).

The analytical data from the DoE experiments (Table 3) were evaluated as responses with no obtained model – the data showed no significant difference between RTs including the reference at 6 min for any of the analyzed parameters, pool volume, recovery, aggregates, HCP, and charge variants.

Using the DoE data from Table 2, surface plots (Fig 3) were constructed to visualize the optimal combination of RTs in terms of load time and productivity. Close to 40% productivity increase was realized when utilizing variable loads of 1.6, 3.5, and 6 min (Fig 3B).



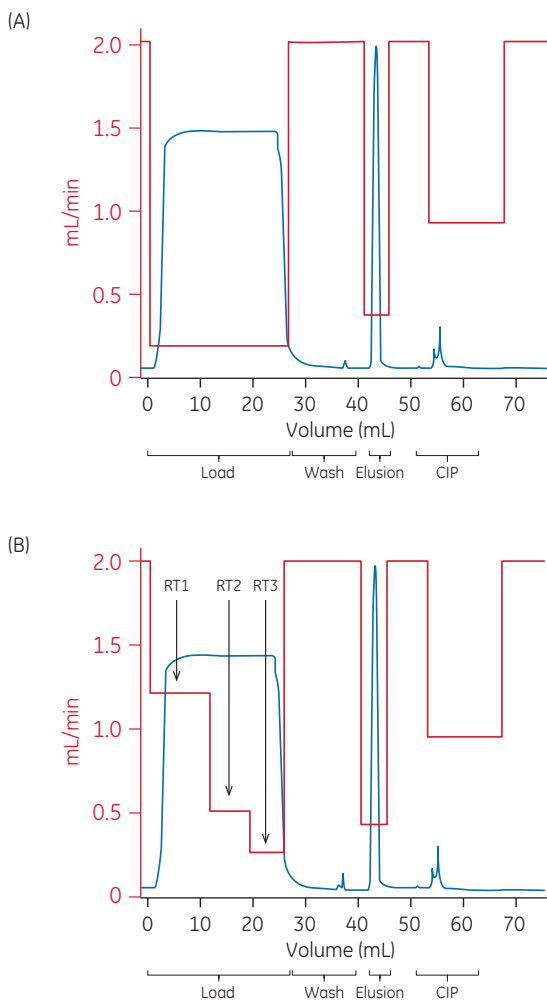
**Fig 3.** Surface contour plots of the effects of variable RTs on (A) load time, and (B) productivity increase (%). Two RTs that were varied (x-axis and y-axis) and the third RT was always 6 min. Data from Table 2.

**Table 3.** Analyses of product quality form the DoE experiments

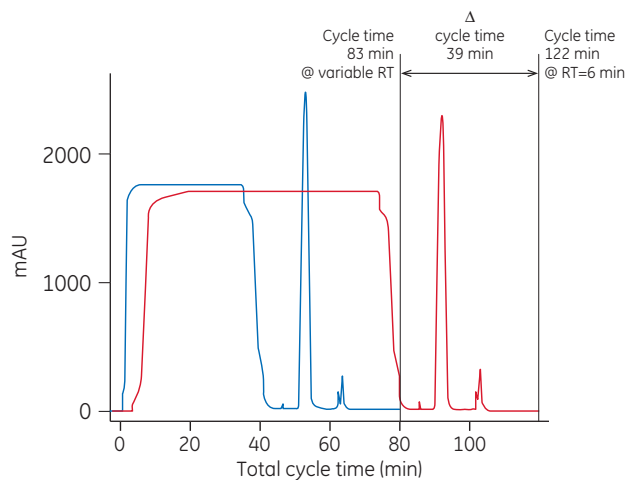
Sample	Pool volume (CV)	Relative MAb recovery (%)	Relative aggregate (%)	Relative HCP (ppm)	Charge variants		
					Acidic (%)	Main (%)	Alkaline (%)
Reference at 6 min RT	1.5	94	0.9	1092	60	34	5
N1	1.4	95	0.9	995	62	34	5
N2	1.4	96	1	1004	62	33	5
N3	1.5	98	1	941	63	33	5
N4	1.4	96	1	904	62	33	5
N5	1.5	96	1	963	62	33	5
N6	1.4	100	1	1074	62	33	5
N7	1.4	100	1	1076	63	32	4
N8	1.4	99	1.1	1003	63	33	5
N9	1.4	100	1.1	949	63	32	5
N10	1.4	94	1.2	1059	64	32	4
Design, mean	1.42	97	1.03	997	62.6	32.8	4.8
Design, SD	0.04	2	0.08	59	0.7	0.6	0.4

## Investigation of variable RT during load

Figure 4B shows the results of a run using the two shorter, optimized RTs followed by 6 min for the longest RT. Up to 80% of  $Q_{b,10}$  was loaded for each RT. The chromatogram is nearly identical to a reference run with constant loading time of 6 min RT (Fig 4A). Analysis of the elution pools from both runs showed that purification performance was maintained in terms of recovery and HCP levels. However, when the same two chromatograms are superimposed, using time on the x axis (Fig 5), a much shorter cycle time is found for the experiment with the multiple RTs.



**Fig 4.** Chromatogram showing effects of combining different RTs on recovery. (A) Single RT at 6 min during load, and (B) three different RTs, short (1.6 min), intermediate (3.5 min), and long (6 min) during load. The high UV-response during loading is due to breakthrough of impurities.



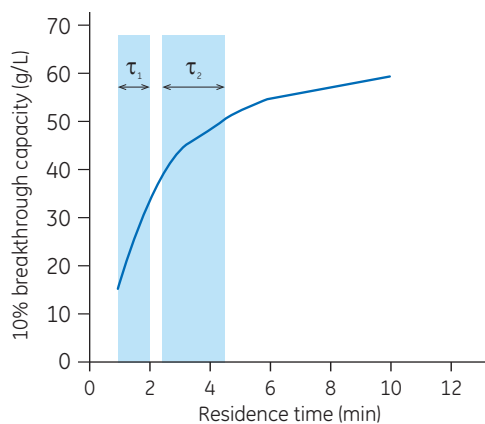
### Maintained recoveries and impurity profile

Pool volume	1.5 CV
Recoveries	> 95%
Aggregates	1%
HCP	~1000 ppm
Ligand leaching	3 to 7 ppm

**Fig 5.** Superimposed chromatograms from Figure 4 but using total cycle time on the x axis. Note that a significantly decreased cycle time was achieved, while maintaining recovery, aggregate and HCP levels, and leaching.

## Theoretical modelling

When the shape of the curve of DBC versus RT has been determined (Fig 2), it is possible to calculate the optimal RTs without doing extensive optimization/DoE analyses. Figure 6 shows the parameters used to construct a theoretical model of optimal RTs, using DBC at different RTs and resulting cycle time calculations.



### Variable residence time ( $\tau$ )

$\tau_1$	1.2 to 2.0 min
$\tau_2$	2.5 to 4.5 min
$\tau_3$	Fixed at 6 min

**Fig 6.** Theoretical modelling parameters used in the calculation of optimal RTs. Note that the RTs were kept at intervals similar to those in the experimental studies. Blue areas show variable residence times.

DoE methods similar to those in the experimental studies were used to construct a surface contour plot for productivity increase (Fig 7). The results of the theoretical modelling were remarkably similar to those in the experimental study (Table 4), showing that knowledge of the DBC versus residence curve characteristics allows for accurate theoretical calculations, without extensive optimization/DoE modelling effort.

## Conclusions

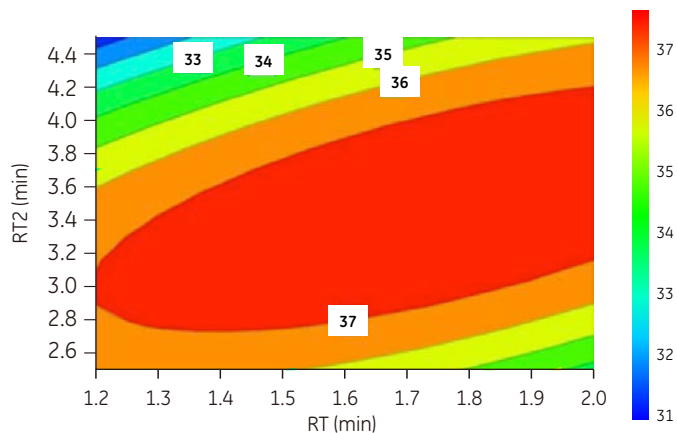
MabSelect SuRe LX is a high capacity protein A medium that can bind approximately 60 g/L IgG. To best utilize its high capacity, the medium should be operated at 6 min RT. In order to maximize productivity one would like to achieve high capacities for MabSelect SuRe LX while operating at shorter RTs. The goal of this study was to assess the possibility of using variable RTs to increase productivity for MabSelect SuRe LX, while maintaining capacity and performance.

By dividing the loading phase and using different flow rates for each phase, the average RT can be shortened while capacity is kept nearly constant. In this study, the longest RT was fixed to 6 min in order to compare it to a reference standard load with a single RT of 6 min. The shortest RT was set to 1.2 min, which is determined by the pressure flow properties of the medium (500 cm/h or 1.2 min RT for 10 cm bed height). A design was created where the shortest RT was varied between 1.2 to 2 min followed by an intermediate RT from 2.5 to 4.5 min and a final RT of 6 min. For each RT the column was loaded to 80% of the DBC at 10%. The result from this design proved that the average RT could be shortened to 2.9 min, with capacity similar to that for a single RT at 6 min. This resulted in a productivity increase of almost 40% relative to the reference RT.

Utilizing variable RTs can significantly increase productivity, while maintaining capacity and purification performance. Theoretical modelling, constructed with knowledge of the DBC vs RT curve, showed nearly identical results to the experimental study.

## References

1. Ghose, S. *et al.* Use and optimization of a dual-flowrate loading strategy to maximize throughput in protein-a affinity chromatography. *Biotechnol. Prog.* **20**, 3, 830–840 (2004).
2. Zhang et al, Maximizing binding capacity for protein A chromatography, *Biotechnology Progress* **30**, 6, 1335–1340 (2014)



### Variable residence time ( $\tau$ )

$\tau_1$	1.2 to 2.0 min
$\tau_2$	2.5 to 4.5 min
$\tau_3$	Fixed at 6 min

### Optimized conditions

First RT	1.8 min
Second RT	3.5 min
Third RT	Fixed at 6 min

**Fig 7.** Surface contour plot for optimization of productivity increase using MabSelect SuRe LX, based on theoretical modelling.

**Table 4.** Comparative model parameters from the experimental and theoretical analyses of variable RT on productivity increase

Residence time	Model	
	Experimental (min)	Theoretical (min)
$\tau_1$	1.6	1.8
$\tau_2$	3.5	3.5
$\tau_3$	6	6
Productivity increase	38%	38%

## Ordering information

Product	Quantity	Product code
MabSelect SuRe LX	25 ml	17547401
	200 ml	17547402
	1 l	17547403
	5 l	17547404
	10 l	17547405

## Related literature

### Data files

MabSelect SuRe	11001165
MabSelect SuRe LX	28987062
Biacore Sensor Chip Protein A	29146699

### Application notes

Lifetime performance study of MabSelect SuRe LX during repeated cleaning-in-place	28987296
Dynamic binding capacity study on MabSelect SuRe LX for capturing high-titer monoclonal antibodies	28987525
MAB capture step development using MabSelect SuRe LX	29008129

### Handbooks

Antibody Purification, Principles and methods	18103746
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